Zwick testXpo 2019

Capillary Rheometry – A Method to Predict Flow Properties under Processing Conditions

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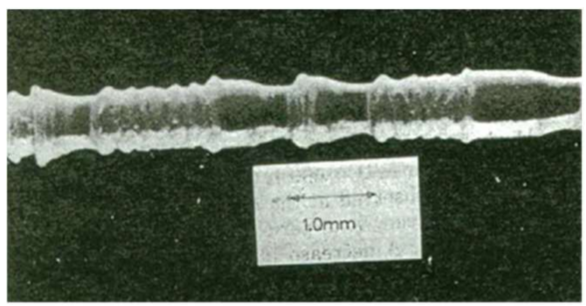
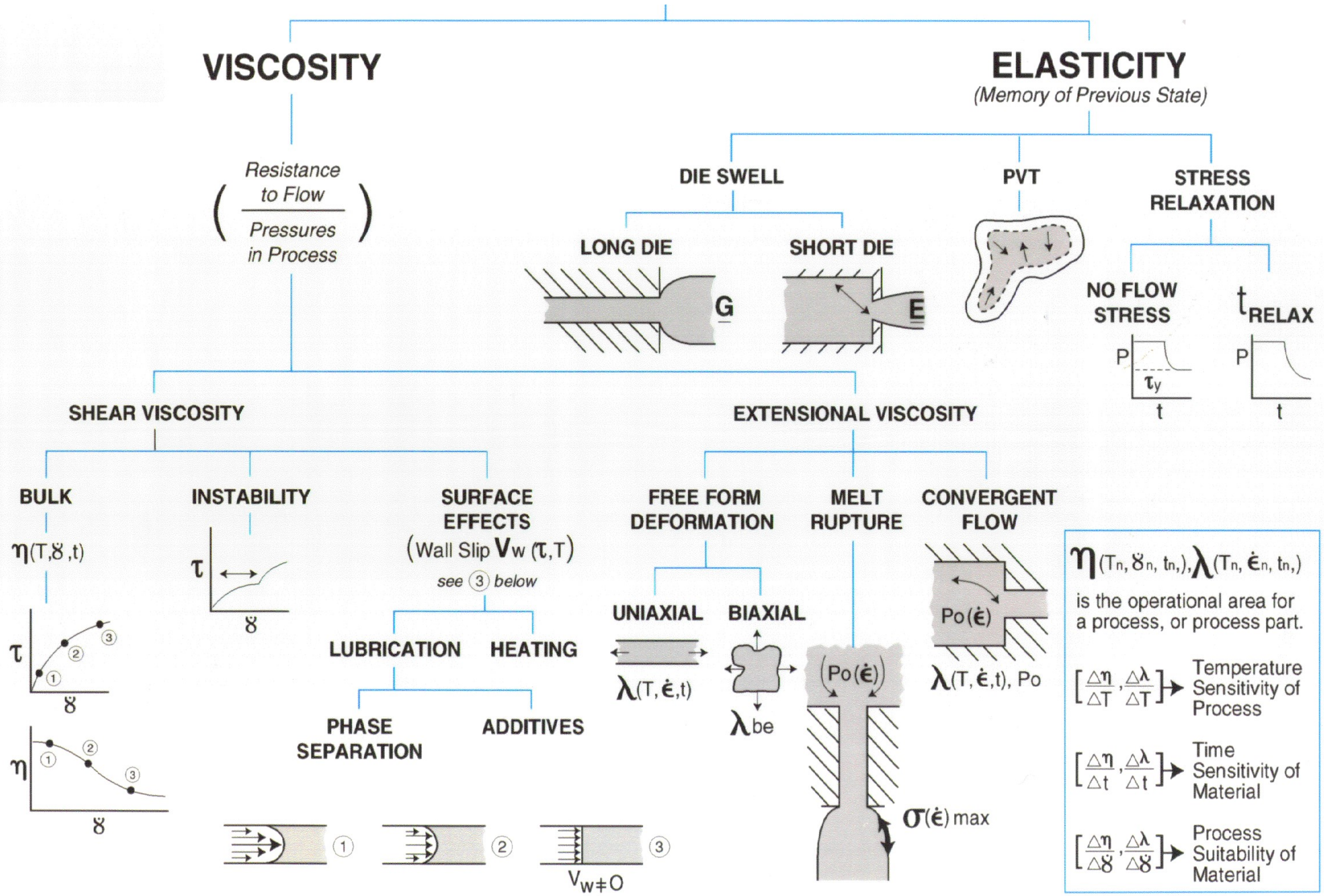


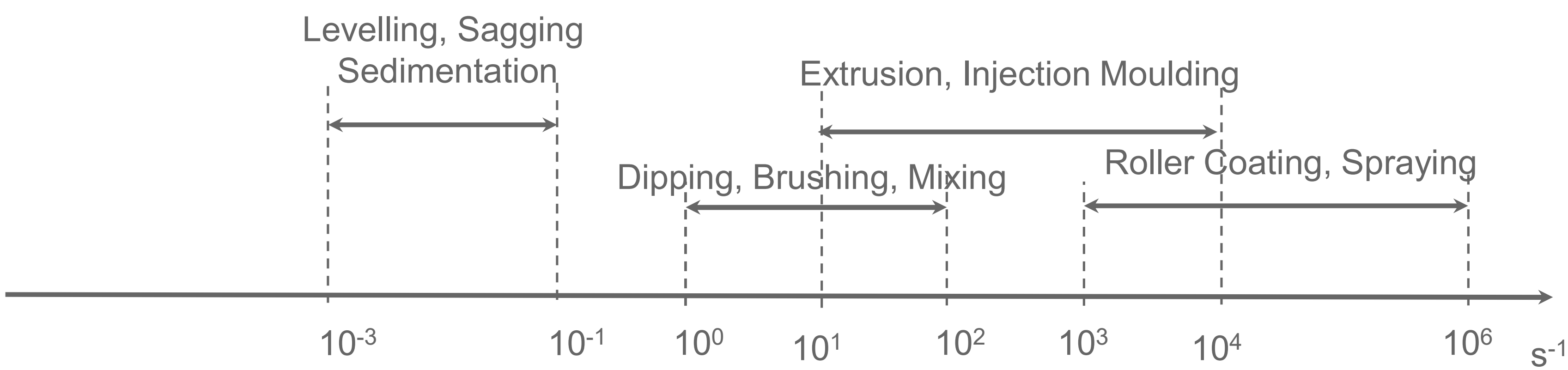
Overview

- Range of Applications for Capillary Rheometry
- Introduction into capillary rheometry: Principle of Operation and theoretical background
- Test results on LDPE: Complete Capillary Characterisation
- Detection of Flow Instabilities
- Advanced Test Types

Capillary Rheometry: Main Applications



Typical Shear Rates



Rotational-Rheometer

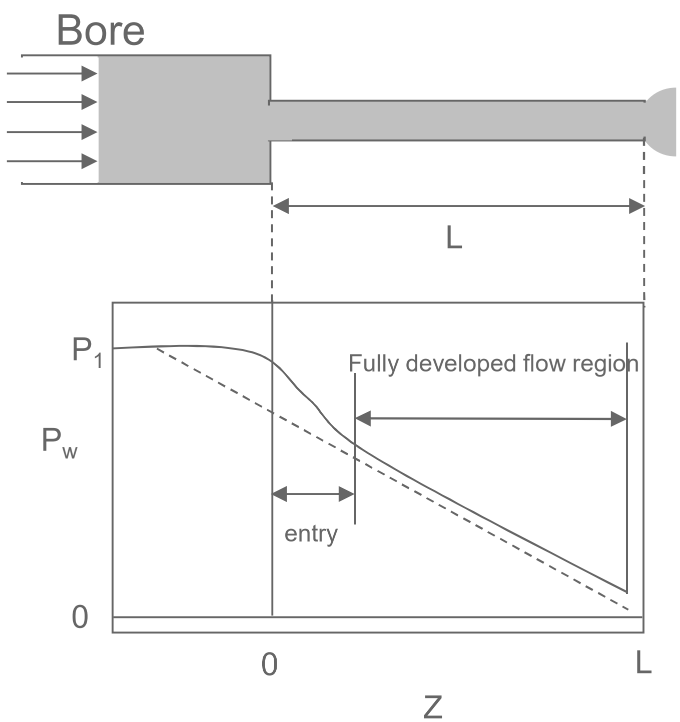
Sample: Water up to solids
Results: Shear-Viscosity, Yield Stesses, Visco-Elasticity, Relaxation...

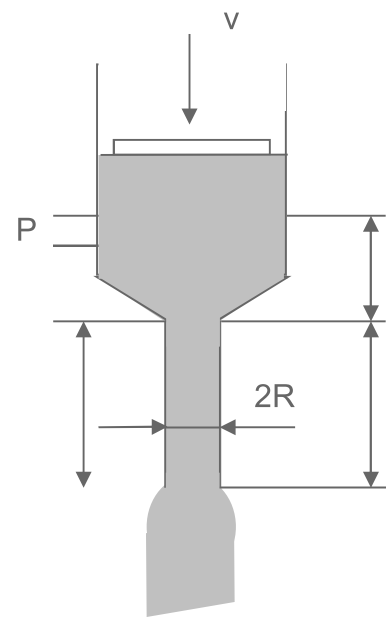
High Pressure Capillary-Rheometer

Sample: Water up to high viscous
Results: Shear-Viscosity, Elongational-Viscosity, Wall Slip...

Principle of Operation

Given quantity:	piston speed	⇒	wall shear rate
Measured quantity:	pressure drop	⇒	wall shear stress





Full pressure drop

=

Entrance pressure drop

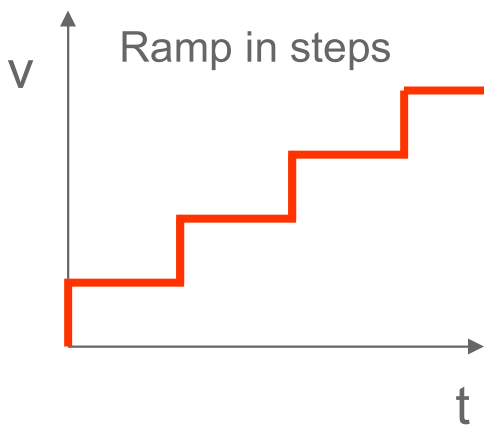
+

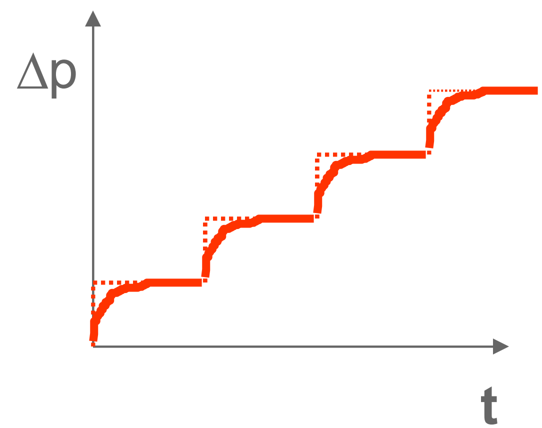
Shear pressure drop

⇒ small ram extruder

What are we doing to get flow curves?

measurement :





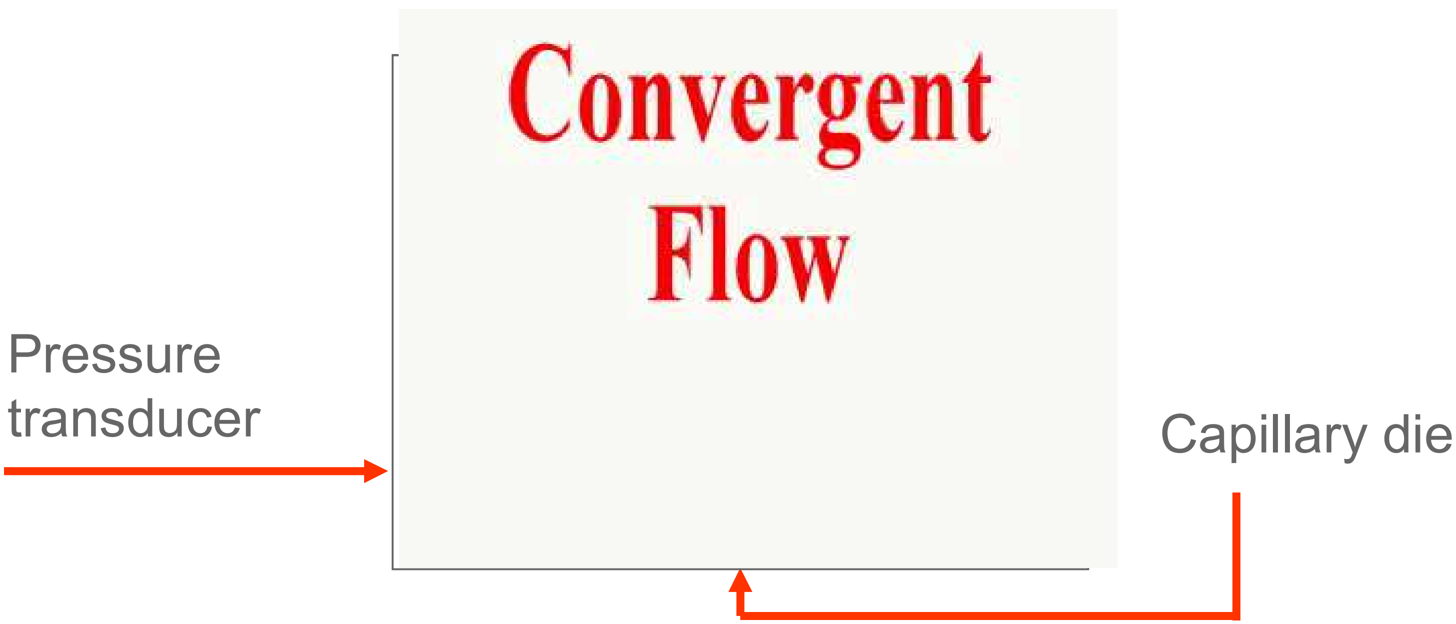
$$\dot{\gamma}_{app} = \frac{4 \cdot Q}{\pi R^3}$$

$$\sigma_{app} = \frac{R \cdot \Delta P}{2 \cdot L}$$

corrections →

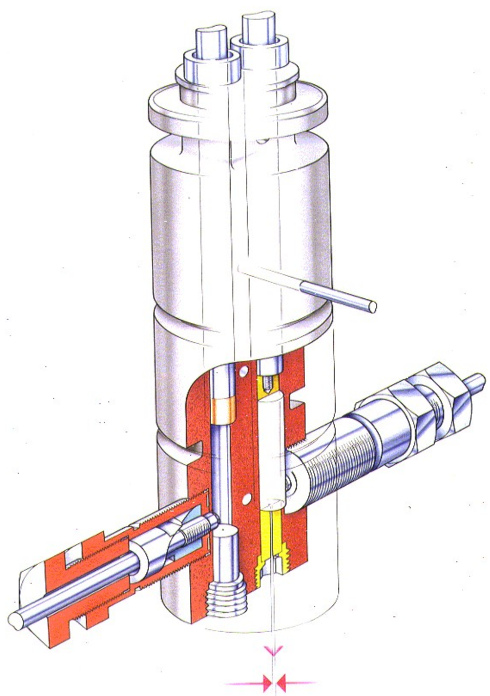
$$\eta = \frac{\sigma_{true}}{\dot{\gamma}_{true}}$$

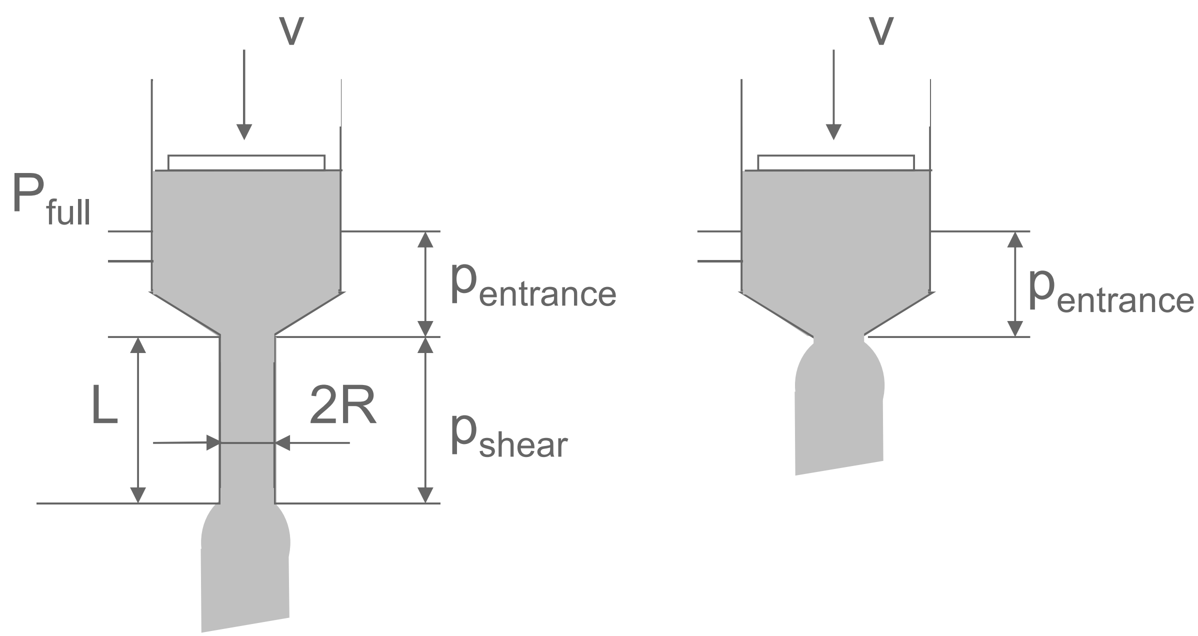
Correction:
Entrance zone of a capillary die



Aim of the test: to separate entrance pressure and shear pressure drop!

Rosand Twin Bore Principle





$P_{full} = P_{shear} + P_{entrance}$

left: capillary

right: orifice

How do we get the Extensional Viscosity?

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Cogswell`s Convergent Flow Model $\Rightarrow$ Extensional Viscosity

$$P_{full} = P_{shear} + P_{entrance} \longrightarrow \lambda = \frac{9\,(n+1)^2\,(P_e)^2}{32\,\eta\,\dot{\gamma}^2}$$

- **Special Orifice Die according to Uni Zlin Model enables characterisation of very small extensional rates too.**

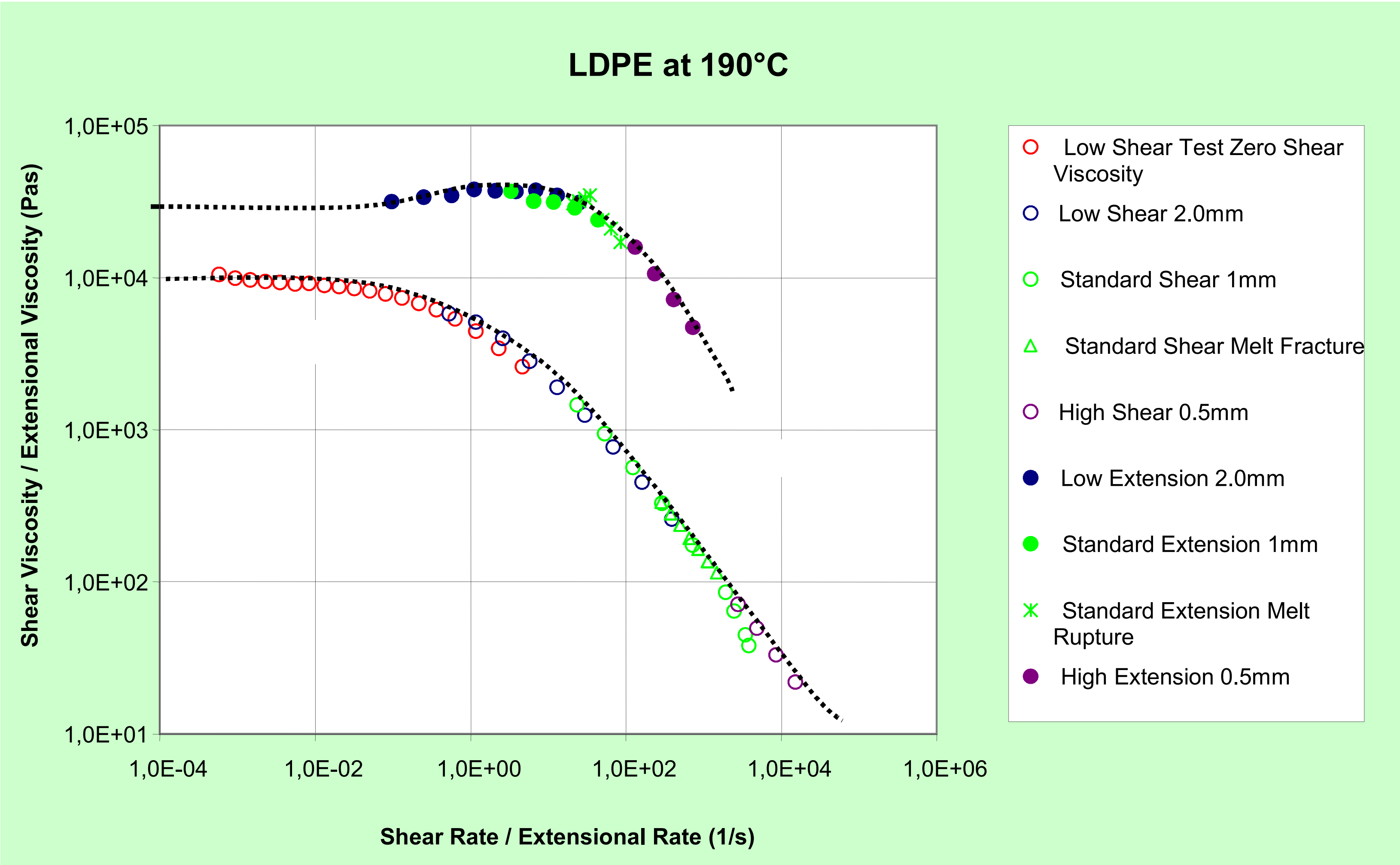
$$n = \frac{d\,(\log \sigma)}{d\,(\log \mathring{\gamma})}$$ Non-Newtonian Index (Ostwald-de Waele)

$$\dot{\varepsilon} \approx 10^{-1} - 10^{3}\ s^{-1}$$

F. Cogswell, “Polymer Melt Rheology”, Woodhead Publishing Limited (1981)

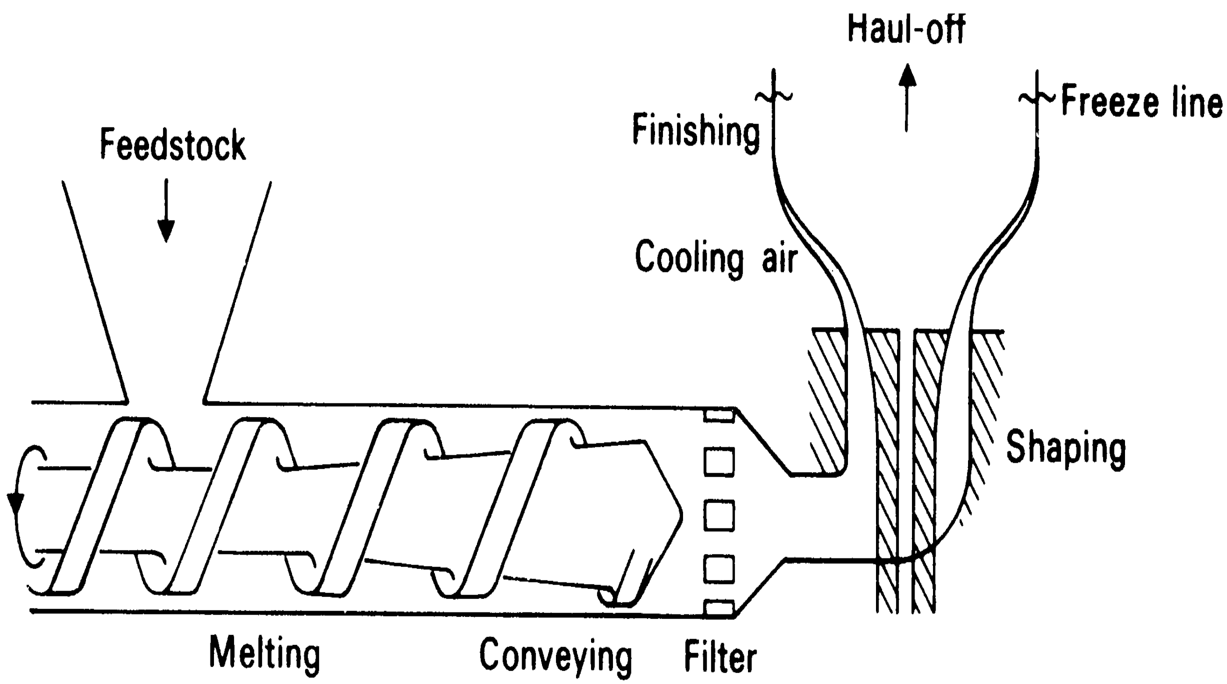
Zatloukal, Vlcek, Tzoganakis, Saha *J. Non-Newtonian Fluid Mech*. **107** (2002) 13–37

Example LDPE



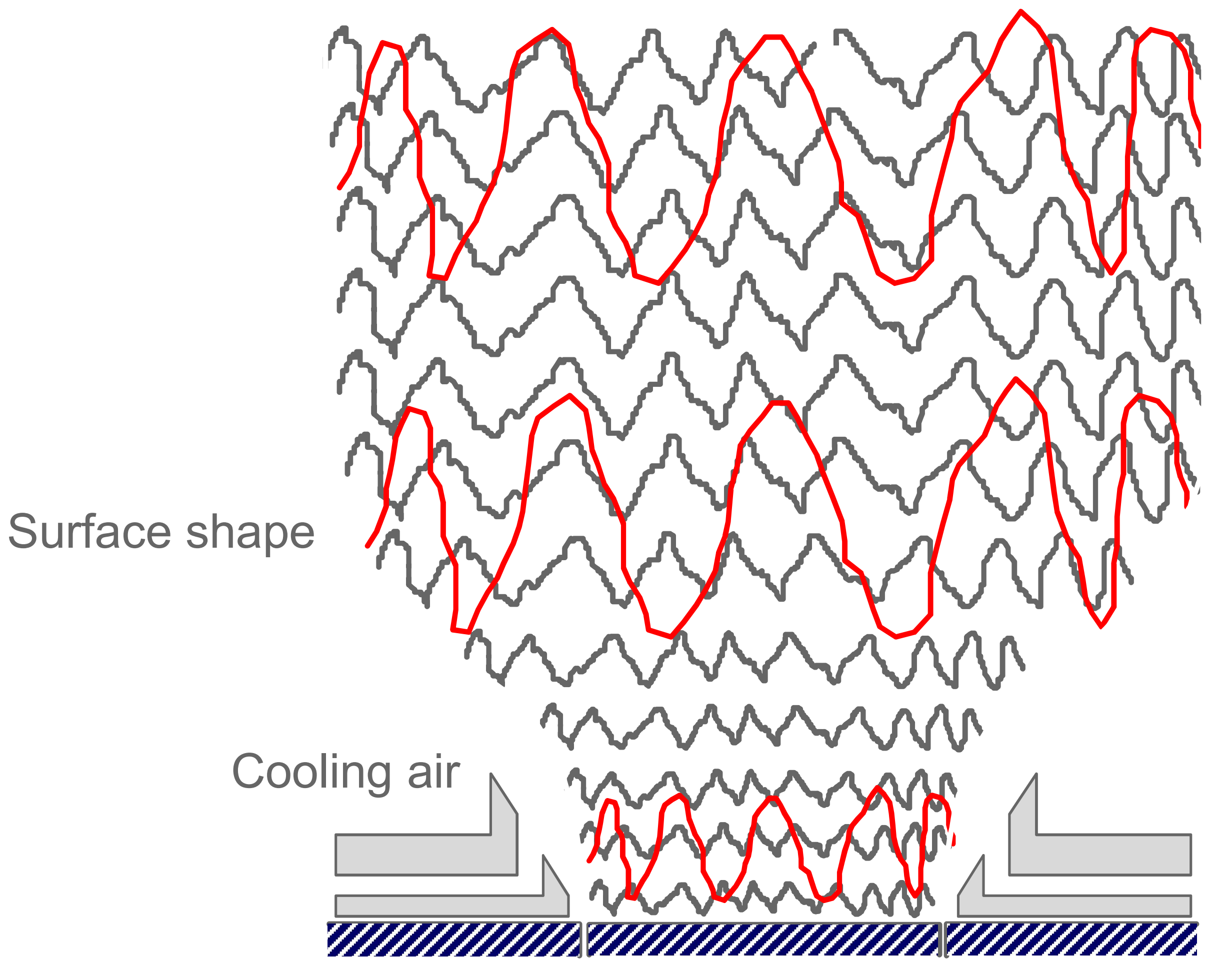
Extensional Rheology of LDPE

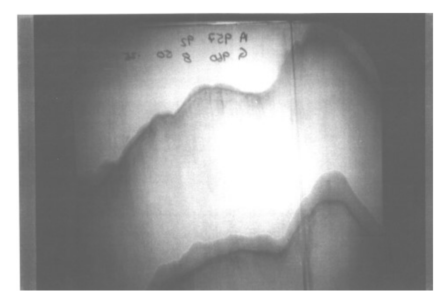
Blow Moulding



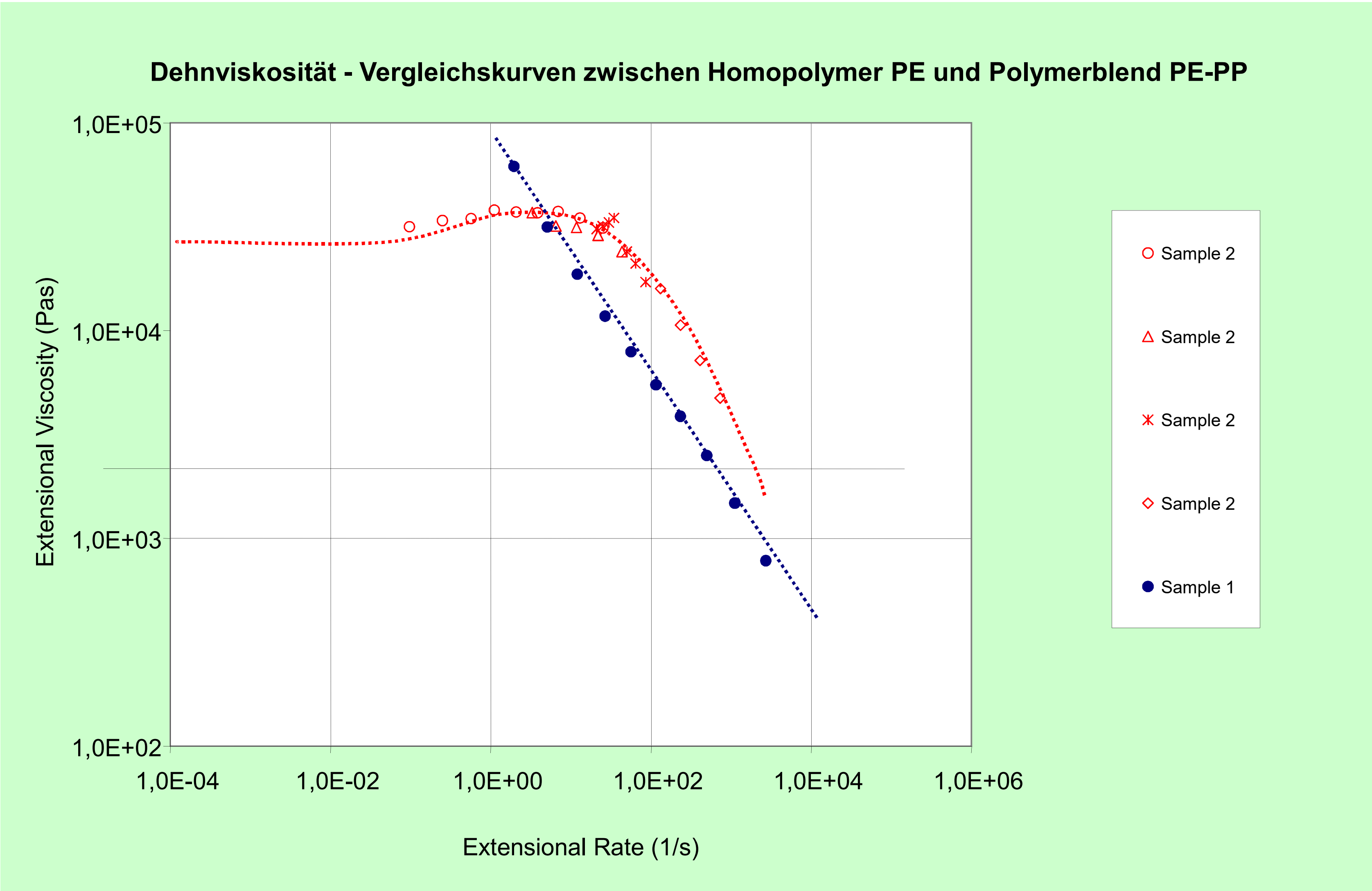
⇒ Blow Moulding is mainly influenced by Extension!

Surface Instabilities LDPE





How can the process be improved?



LDPE in Co-Extrusion Die

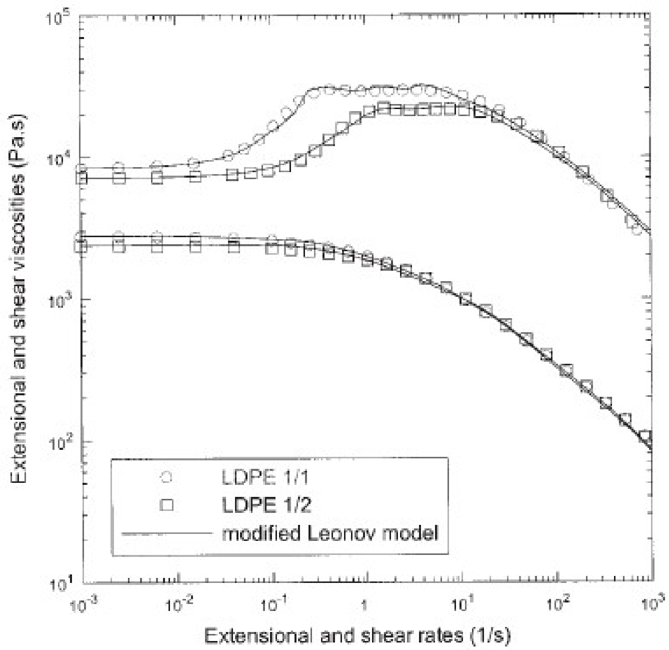


Figure 4 Extensional and shear viscosities for two different lots of LDPE 1, 210°C.

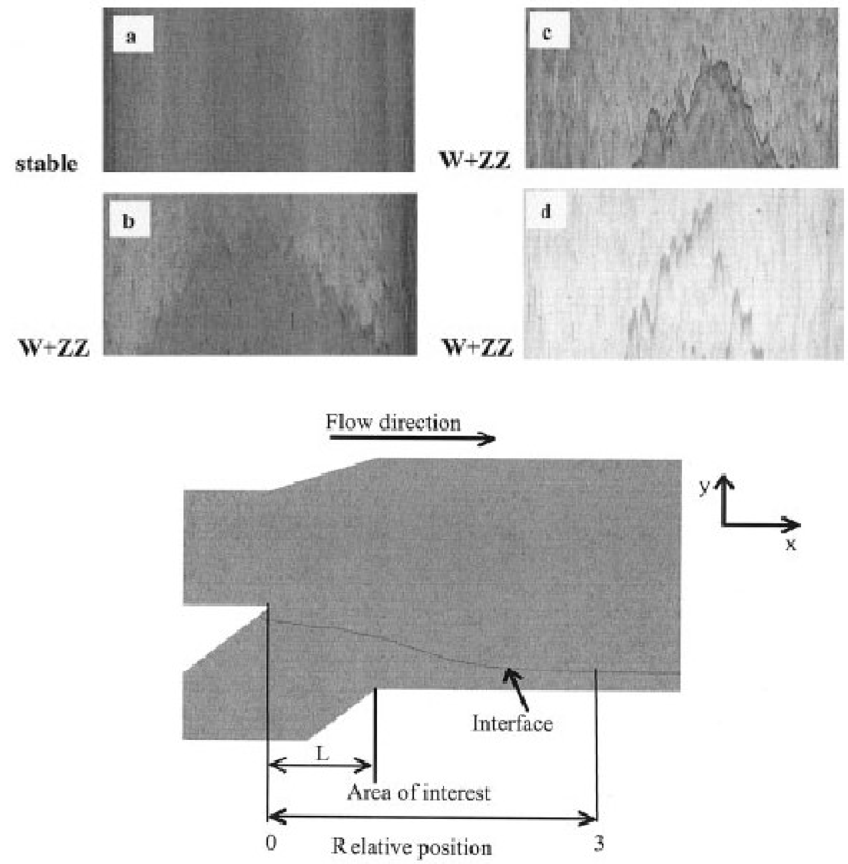


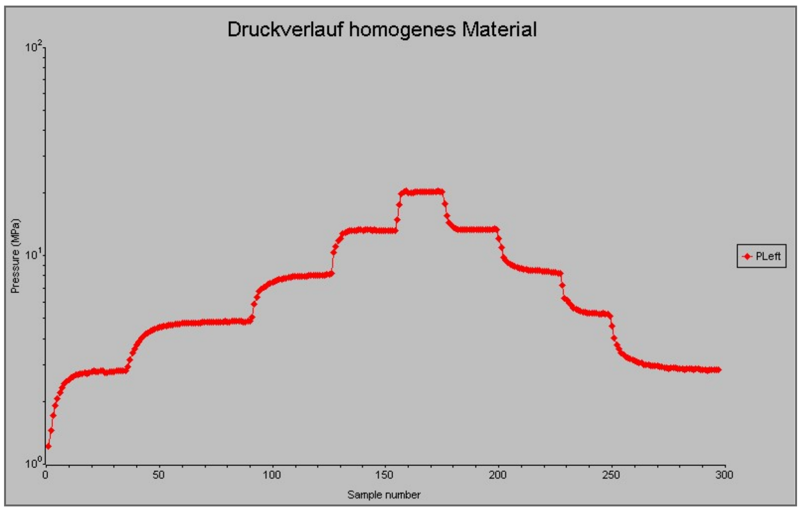
Figure 5 Merging area of the flat coextrusion die.

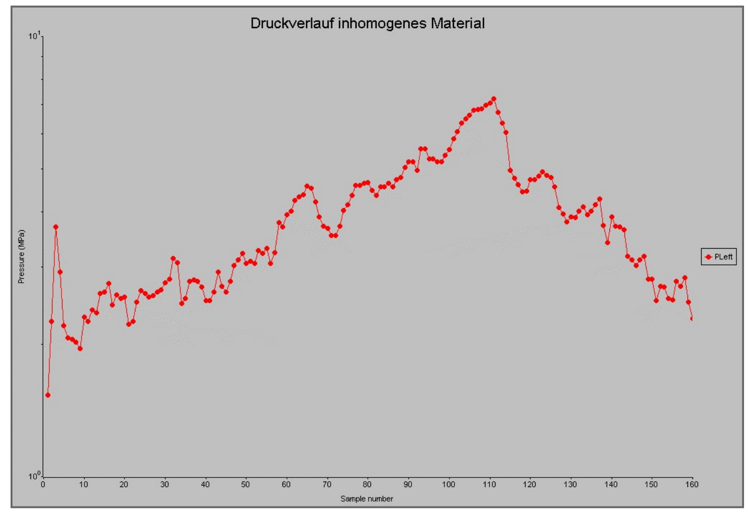
Instabilities caused by Extensional Flow Behaviour of LDPE

*Zatloukal et. al. Journal of Applied Polymer Science, **98** (2005) 153*

Equilibrium Pressure: Homogeneity

Pressure drop is important





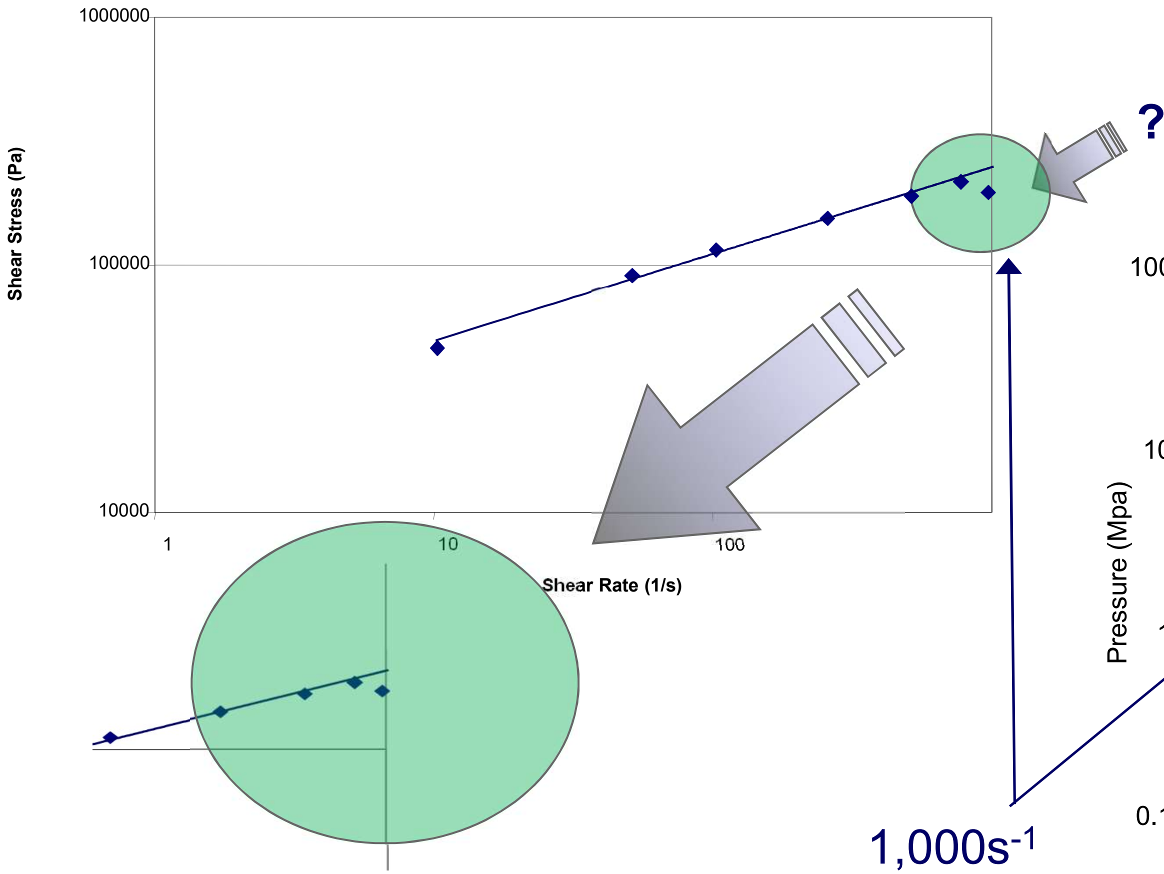
homogeneous

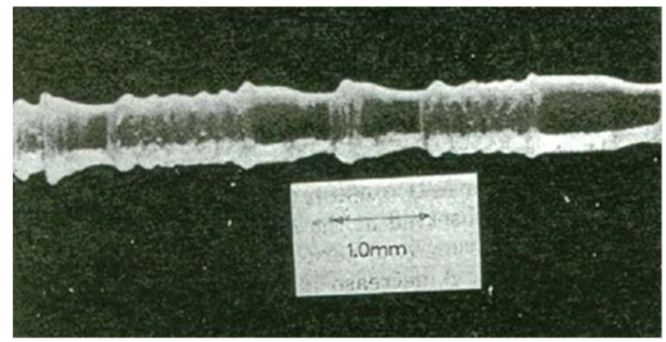
inhomogeneous

⇒ For polymer blens, filled polymers, suspensions, emulsions, composites etc.

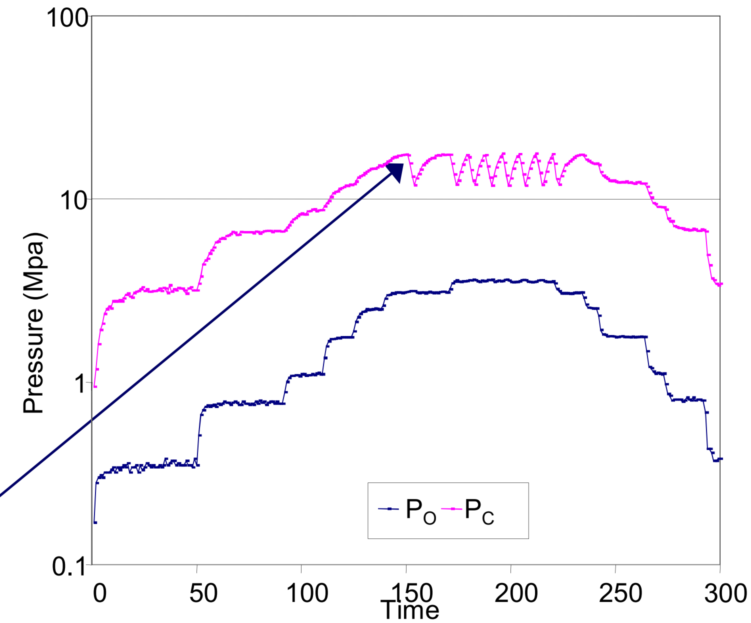
Melt Fracture

- Unstable flow, poor product quality.





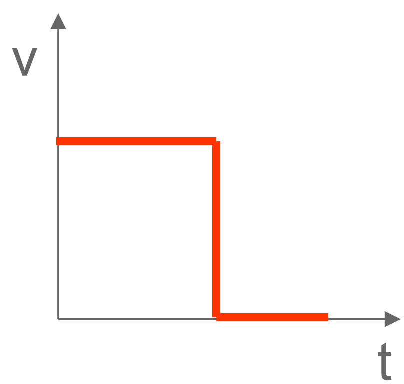
1,000s^{-1}

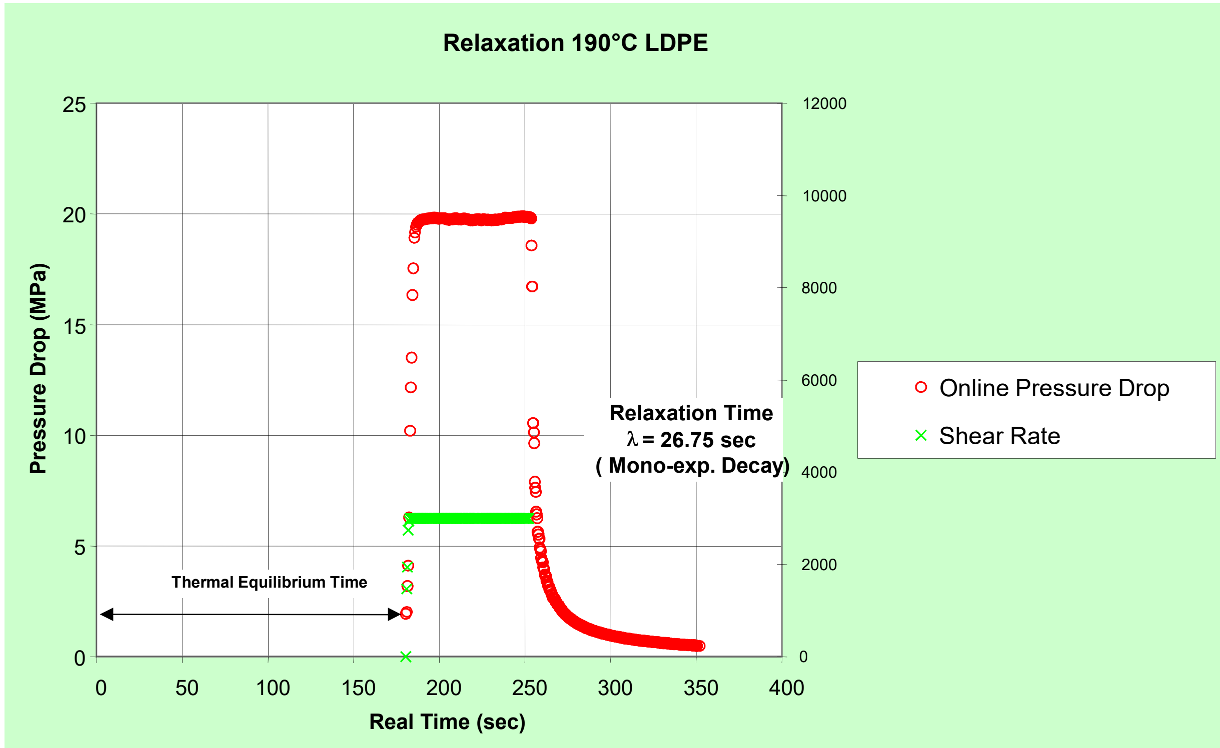


Relaxation LDPE

What happens after processing

Prinzip:

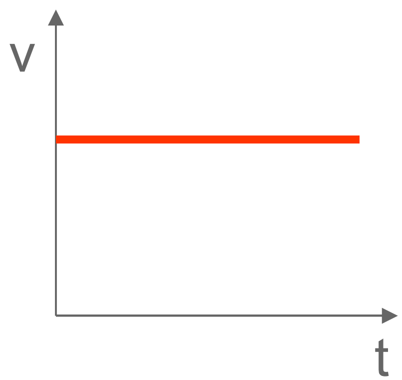


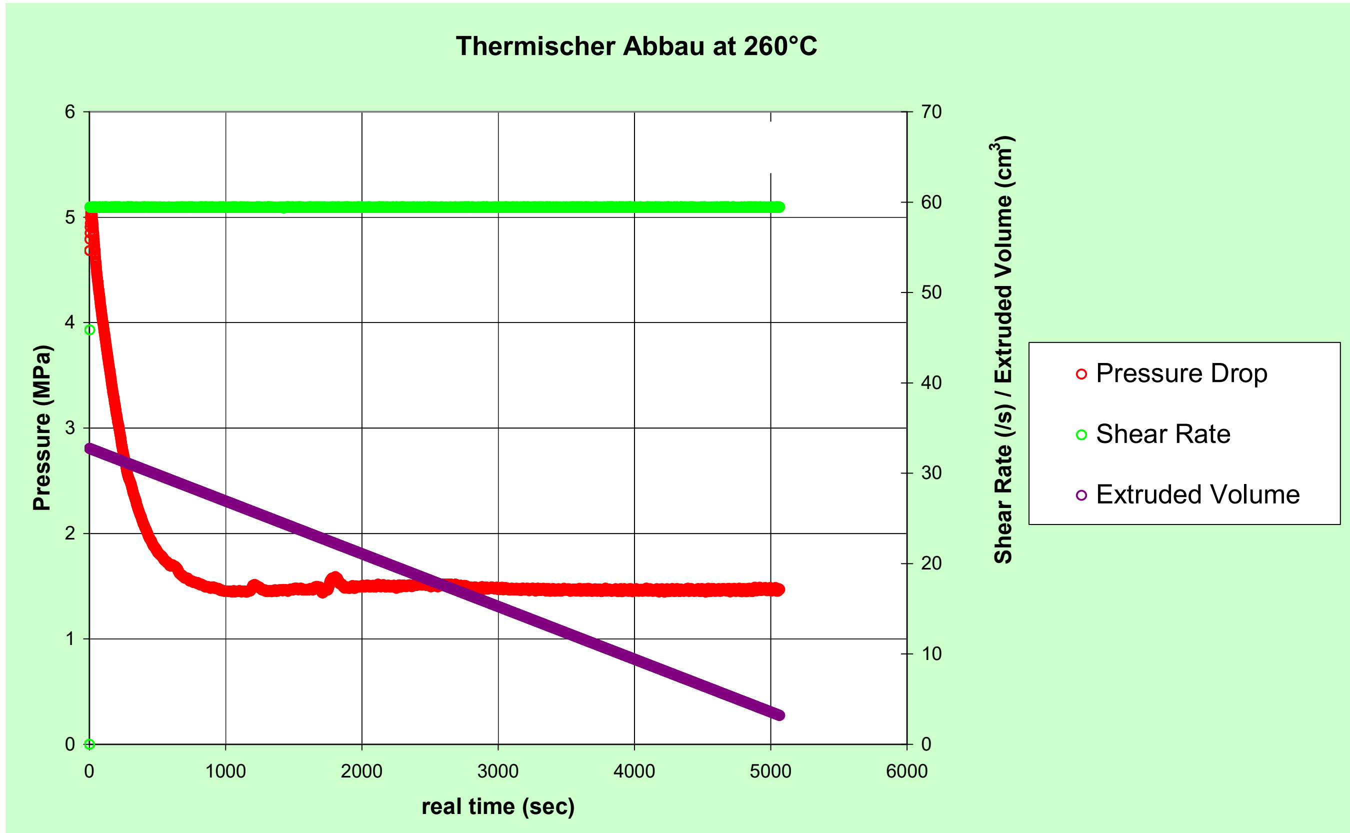


⇒ inner stresses can lead to surface crack (automotive industry)

Thermal degradation / Curing

Prinzip:





⇒ Gives maximum process times under high temperatures

Rheometer Types

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Benchtop RH2000 and Floor Standing RH7/10

Summary

- Capillary Rheometry gives correlation with processing flow properties
- Calculation of extensional viscosity according Cogswell method
- Flow curves up to very high shear end extensional rates
- Prediction of flow instabilities
- Correlation with structural changes during processing

Thank you for your attention.

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